

Flexible Operation of Steam Power Plants

Solutions from SIEMENS ENERGY

Ian Rebello 22nd November 2022 Kolkata



Changing energy market



	SOLAR WIND		COAL & LIGNITE
2012 CEA	21	GW	125
2022 CEA	114	GW	210
20 <mark>32</mark> Niti Aayog	500	GW	200 More Retirals Less Additions
2047 Niti Aayog	650	GW	333

Coal based power plants – will have to become

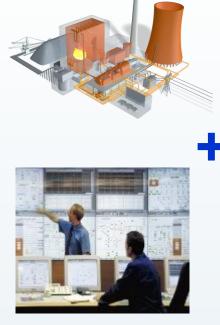
- Agile
- Handle minimum loads
- Improve efficiency
- Lower emissions to remain operational





Siemens Power & Process Automation Modern control concepts for high profitability





Process engineering competence

600 GW installed, 10 GW operated by Siemens

Automation competence

2500 systems based on proven Siemens technology



Power-IT competence

Role-based information supply for everyone in the power plant Excellent control concepts form the basis for Process Optimization solutions:

- Model-based, predictive feed forward structures
- Decoupling of highly intermeshed sub processes
- State space control
- Neuronal networks and fuzzy logic

This makes it possible to achieve extremely stable, reproducible and flexible operating behavior -

The basis for high profitability

Siemens approach to reduce min. load up to 40% There is no One Size Fits All !!!

to full load will be

Siemens-Energy.

analyzed from



Implementation and

automation of min. load **Providing of** Reducing min. Alignment on load on site **Process Data** min load tests Answering Questionnaire Siemens Energy implements the Siemens Energy identified measures to Siemens Energy suggests based on Process data from automate the load experts and the the provided Information about one cold start-up, one reduction and secure a operators from the information and the thermal state of plant ramp down to min stable operation during power plant reduce result of the data (degradation level), load and one ramp up min load the min load according analyzation a test existing automation

procedure to reduce

min load.

the agreed test

obstacle occurs.

procedure until first

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level, flamer scanner,

start-up procedure etc.

combustion stability,

have to be provided

Typical Questions – Identify improvement in specific areas



Plant Configuration

- Boiler type (drum/once through)
- Number of mills ? Mill manufacturer/design ?
- Burner configuration (Tangential, wall, opposed wall, ...)
- Boiler DCS manufacturer / Model ?

Efficiency & Emissions

- How often does the plant perform soot blowing in the economizer /evaporator/superheater / APH area?
- What is the furnace exit temperature ?
- What is the current HP steam temperature set point? & deviation ?
- What are current values for CO?
- What are current values for carbon in ash (LOI)?
- What are current values for NOx ?

<u>Flexibility</u>

- What is the current Minimum Load?
- What is the Minimum Load target for the future? What is the current technical limitation for more ? Minimum Load ?
- Would a higher part load efficiency add business value?
- Is it lucrative for the plant to increase the range of frequency control?
- What are the current load ramps?

Siemens approach to reduce min. load Example - Test Plan



Time (IST)	Time (CET) Lo	ad	Status	Procedure	Observation
			1	Min load, unit control normal operation, mills B-		
				E in operation, one feedwater pump already out		
				of operation (if possible), SCAPH already in	Select burner tilt, O2 and main steam pressure as found most suitable in	
10:30	(07:00 29	0 MW	operation	last test	
					If not done before: Put SCAPH in operation for increased APH flue gas	
10:30		07:00			temperatures.	
					If not done before: Take feedwater pump out of operation as early as	
					possible, and operate with 1 pump. If possible, before reducing load	
10:30	(07:00			below actual min load.	
					Take mill E out of operation. Operate with the minimum number of mills	
10:30	(07:00			(three) that are required for this load. Use mills B, C and D.	
					Lower load slowly and in steps by adjusting the unit control setpoint. Load	
					changes should be around 25 MW (equaling 5%). This can be achieved by	
					reducing the load setpoint from 288 MW to 263 MW to 243 MW to 220	
					MW to 210 MW, using a slow slope (e.g. 0.5%/min). After each load	
11:30	(08:00 29	0 MW		reduction, wait about 30 minutes for stabilization	Drum level, SH&RH steam temperatures, combustion,
					After each load reduction, wait about 30 minutes for stabilization	Identify process instabilities.
					If no instabilities, reduce load further	Drum level, SH&RH steam temperatures, combustion,
					When instabilities can not be eliminated, go back to last safe load	
11:40		08:10 26	3 MW		Reach 263 MW	
12:10	(08:40 26	3 MW		Setpoint to 243 MW	
12:20	(08:50 24	3 MW		Reach 243 MW	
12:50	(09:20 24	3 MW		Setpoint to 220 MW	
13:00	(09:30 22	0 MW		Reach 220 MW	

Technological solutions to address the challenges



Solutions	Benefits		
 Boiler → Slow-acting Turbine → Fast-acting Solution: Enhanced Unit Controller that ensures better Coordination Optimized Control of Key Operational Parameters → (a) Reheat Temperature b) Main SteamTemperature (c) Flue Gas (d) Feedwater circulation 	 1. Higher Load Ramps 2. Minimum human intervention 3. Improved Plant efficiency 4. Stable Operation at <i>"new"</i> sustainable minimum load 		
Smart Regulation of key Aux Equipment • Fans • Pumps • Mill Scheduler → coal mills	 1. Improved Plant efficiency 2. Auxiliary Power consumption optimized. 3. Minimum Operator intervention. 		
Thick-walled boiler components are impacted with load ramps / thermal cycling. Fatigue life must be monitored. This is achieved through - Fatigue Monitoring System to monitor and determine residual lifetime.	Plant shutdowns can be planned to rectify / replace highly stressed components at the appropriate time – savings in unplanned outages		

Omnivise P3000 Minimum Load Reduction Reduced minimum load level



Task

To upgrade the plant so that the specified minimum load level can be reduced and to make the plant capable of fast and low-stress load increases on demand in accordance with market requirements.

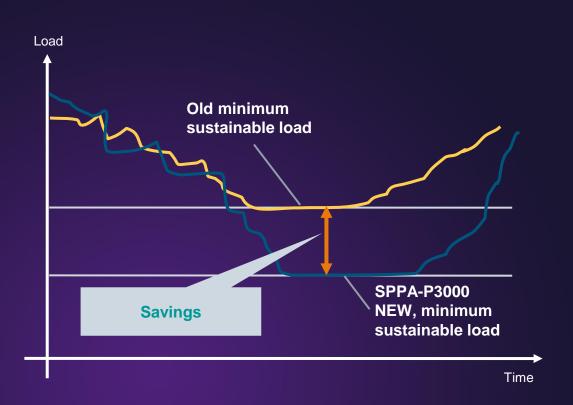
Solution

- Use of robust state space controller for unit control
- Adaptation, optimization and setting of lower-level controls for new minimum load level
- Adaptation or addition of control sequences, burner and mill scheduler
- Provision of additional instrumentation where necessary

Benefit calculation based on

- Reduced financial losses during off-peak periods
- Faster response to increased load demands as unit does not need to be shut down
- Avoidance of unnecessary startups and shutdowns

Minimum Load Reduction

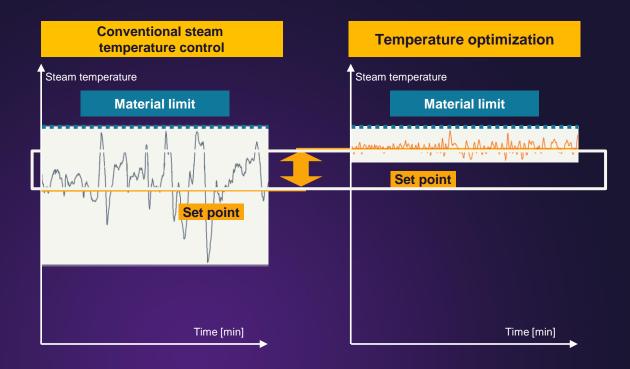


The Minimum Load Reduction solution results in savings for minimum load operation through optimization of lower-level controls.

Omnivise P3000 Temperature Optimizer Increased steam temperatures



Temperature Optimizer



The Temperature Optimizer solution increases the efficiency through higher steam temperatures and the use of appropriate control elements for reheater temperature.

Task

To achieve maximum steam temperature without violation of material limits

Solution

- Robust, easy to parameterize and adaptive state space controller with observer
- Where needed, use of entire control range through to injection into saturated steam
- Use on startup/shutdown and over the entire load range

Benefit calculations based on -

Increased efficiency thanks to

- Higher steam temperatures
- Reduction in reheater attemperation

Omnivise P3000 Sootblower Optimizer Optimized operation of sootblowers



Task

Condition-based, selective operation of individual sootblowers instead of manual or cyclical activation of entire groups of sootblowers.

Solution

Targeted control of key boiler operating parameters such as

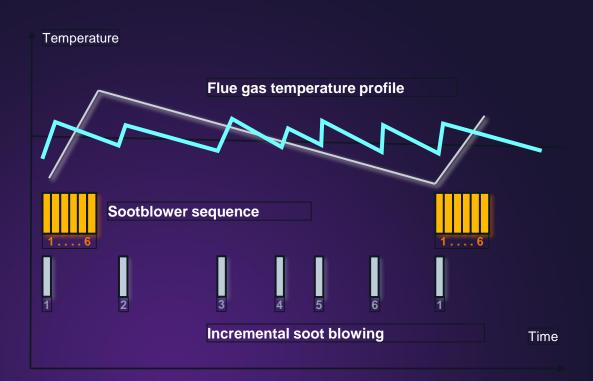
- Reheater attemperation
- Temperature imbalances
- Control range of HP feed water heaters
- Boiler slagging

Automatic activation of individual sootblowers

Benefit calculation based on

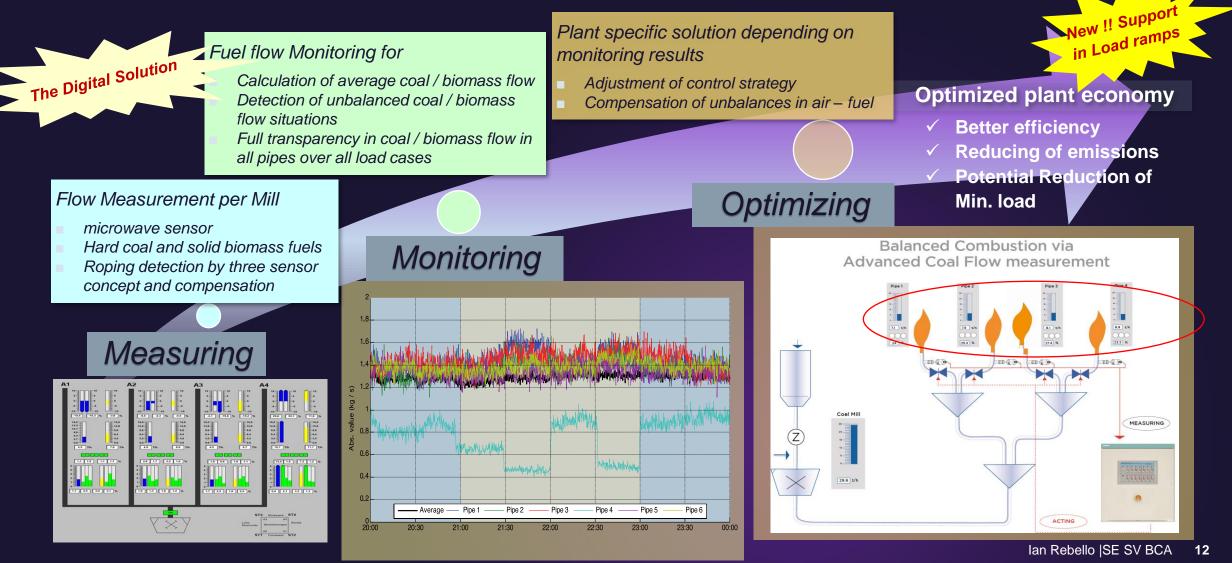
- Reduced fuel costs due to optimal operation of sootblowers
- Higher availability due to avoidance of unnecessary soot blowing

Sootblower Optimizer



The "Sootblower Optimizer" solution enables the optimum operation of individual sootblowers.

Advanced Coal Flow Measurement System The consequent next step : Combustion Optimization

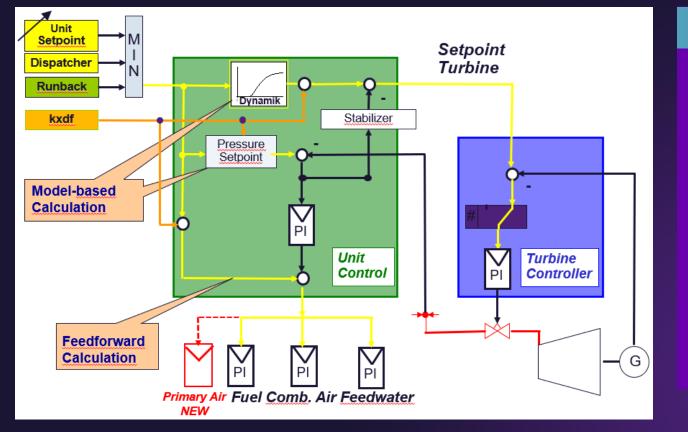


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Coal Flow Measurement System Advantages for Flexibility & Efficiency

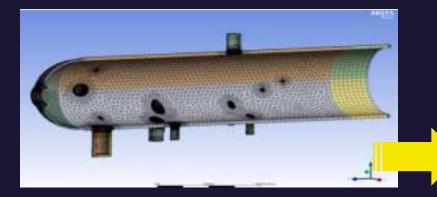




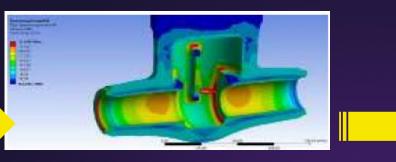
Expected Benefits and Results

- Improved mill and feeder control
- Higher plant stability during load changes
- Higher Load Ramps by using mill storage
- Improved dynamics during fuel demand with new Primary Air Setpoint

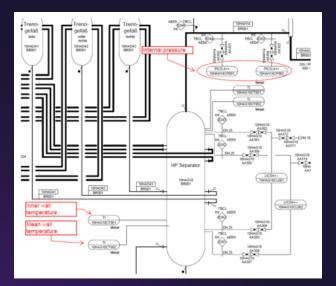
Boiler Fatigue Monitoring System (FMS) Life cycle of Components Online Evaluation--Possible



Online Fatigue calc and evaluation of lifetime limits and stresses



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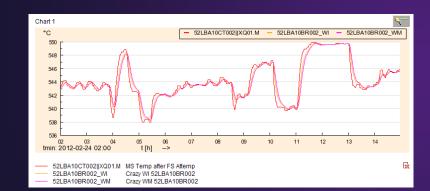


Component under Fatigue caused by Thermal cycling

Affected components:

Headers, Drums, Separator. Attemperators, Piping

How much fatigue is it ? Don't Guess when you can measure it!!!



Optimization of process to regulate the parameters

New fatigue control & Monitoring → Higher flexibility with check on Material Life

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FMS - Overview Max lifetime of components and theoretical lifetime --operating modes

Objective

- Calculation of boiler component's fatigue
- Early detection of deviations

Solution

- Online Determination of creep and low-cycle fatigue of critical components acc to EN 12952
- Online Residual lifetime & Theoretical Limits calculation (No. of cycles to crack initiation)
- > Long term data storage \rightarrow for trends & comparison

Benefits

- Transparency in relation to impact of operating mode on residual life
- Detection and prevention of high-wear operating modes
- Optimum selection of point in time for requisite overhaul and inspection
- Enhanced power plant safety and reliability
- Utilization of component material reserves/spares and better planning.
- Cost-effective in-service monitoring and analysis



Successes in Technical Min assessment and Flexibility Interventions in India





NTPC Dadri 500 MW

Scope

Flexibility Assessment for 500 MW block for technical minimum and ramp rates.

Interventions to automate load reduction to 40%

- Unit Control to coordinate slow-acting boiler and fast-acting turbine
- Reheat / Flue Gas / Main Steam Temperature Control
- Fatigue Monitoring System to determine residual lifetime of highly stressed components
- Replacing of the feed water recirculation valve by a control valve
- Mill Scheduler to switch coal mills on/off automatically depending on the firing demand <u>Next step:</u> Installation of an Online Coal Flow Measurement System



Achieving better part load performance & ramp rates- SPP

525 MW IPP – East India

Scope

Flexibility Assessment for 500 MW block for technical minimum and ramp rates with IGEF and VGB

Customer Benefit

- Technical minimum of 36% established and 3% ramp rates
- Reduced CO₂ footprint



DVC Andal 500 MW

Scope

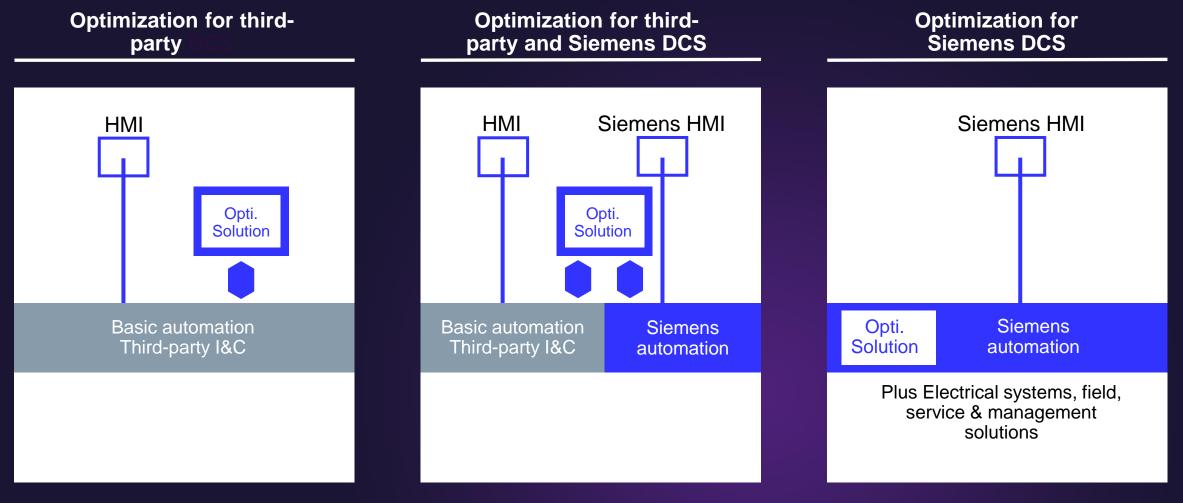
Flexibility Assessment for 500 MW block for technical minimum and ramp rates with IGEF and VGB

Customer Benefit

- New technical minimum of 32% established (country's best) and 3% ramp rates
- Reduced CO₂ footprint

lan Rebello |SE SV BCA **16** Restricted © Siemens Ltd., 2021 Optimization solutions can be used with any DCS and are suitable for new plants and modernization projects



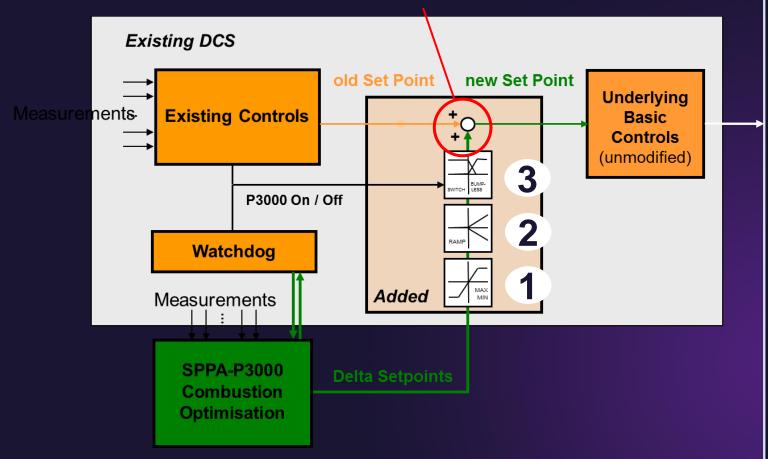


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Interface to the Plant DCS (Non Siemens)



Omnivise Optimization modules typically add a bias to the set point for existing basic controls to be more effective in the process.



Making communication with DCS safe:

- A continuously circulating watchdog signal **monitors communication**.
- => biases are bumplessly fading out on DCS and Onivise side whenever communication fails.

Required **treatment of each incomming biases** from Omnivise in DCS (see drawing on the left):

- Limiting biases to an agreed **minimum** and **maximum**,
- Limiting speed of value change to an agreed **maximum ramp rate**,
- **3** Switching on/off all biases bumplessly within a given time when required (Master switch on/off, communication watchdog fails, ..)

Thank you for your attention!

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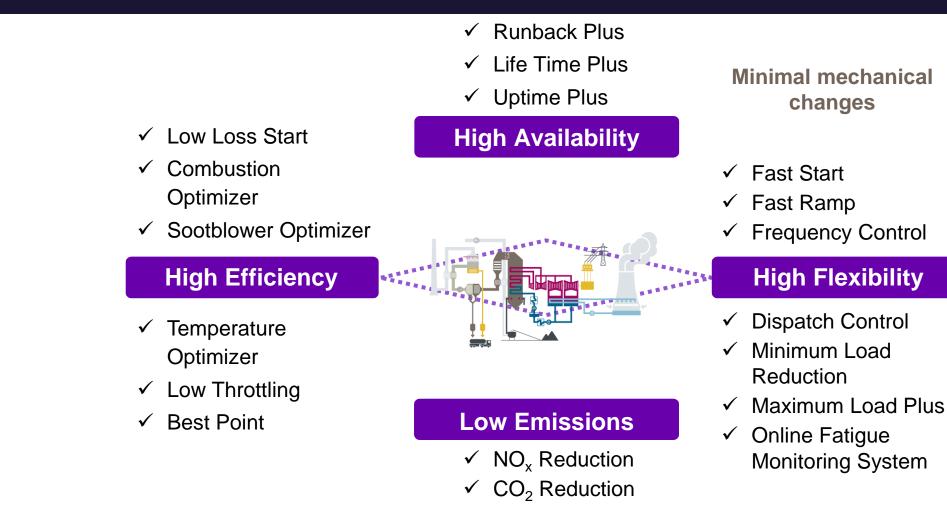
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SPPA-P3000 Frequency Control Increased range for primary frequency control



Task

To upgrade the unit so that it can provide primary frequency control and spinning reserve. Due to the fast load ramps that this service requires, it places very high demands on the dynamic control response of a power plant unit.

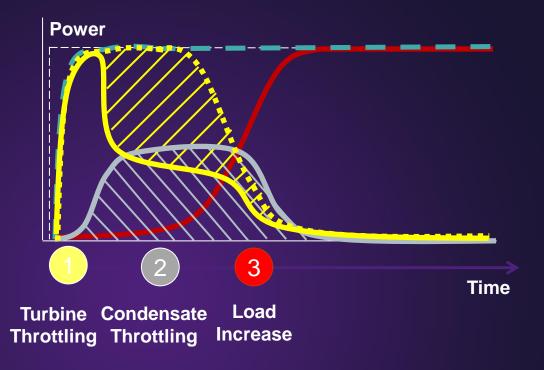
Solution

- Activation of the condensate throttling to mobilize energy storage and/or
- Throttling of turbine valves

Benefit calculation based on -

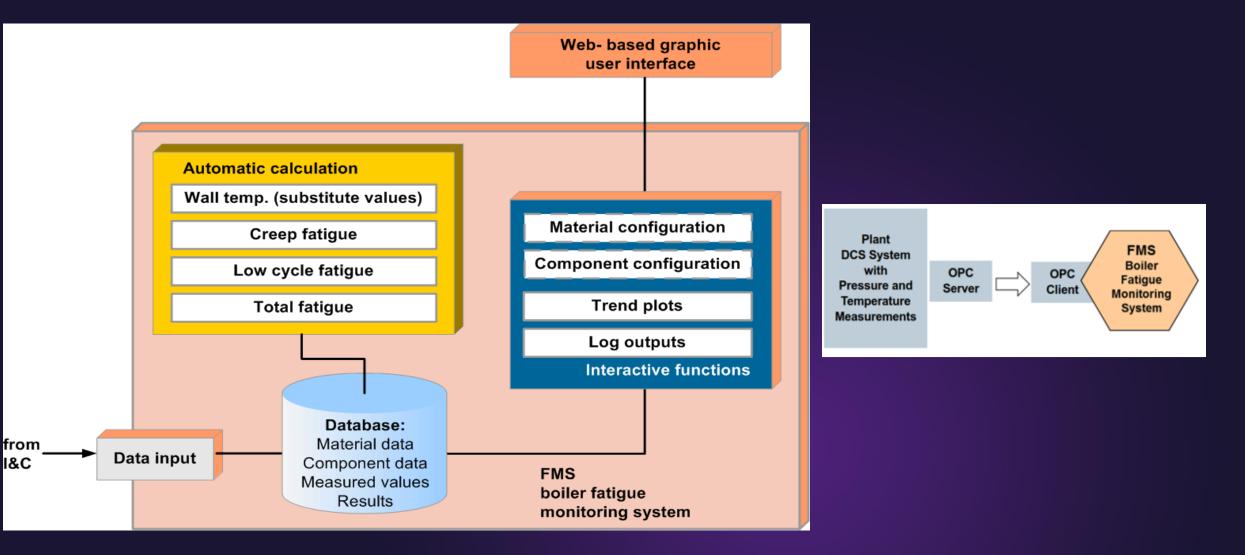
- Increased revenue from primary frequency control and spinning reserve services
- Avoidance of fiscal penalties for non-provision of contractually agreed primary frequency control and spinning reserve services

Frequency Response including P3000 Condensate Throttling (Efficiency):



Boiler Fatigue Monitoring System (FMS) System Architecture





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Power on Demand Monitoring of flexibility consequences: steam turbine EOH counter

Task

- Part load may lead to steam temperature changes, especially hot reheat temperature
- Thermal stresses during operation are not considered in standard counting of equivalent operating hours (EOH counter)
- Maintenance needs may not be recognized

Solution

- Evaluation of operational history
- Implementation of a state of the art EOH counter considering load changes

Benefits

- More accurate EOH counting
- Improved outage planning
- Enhanced operational flexibility

EOH counting also considering load changes

EOH consumption is a function of actual thermal stress

Introduction of three start-up modes with fixed EOH consumption

Maintenance interval defined by operating hours and number of starts

